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# Hiemenz stagnation point flow with computational modelling of variety of boundary conditions



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#### ABSTRACT

This work explains the flow of a  $G-H_2O$  nanofluid under the special case of MHD stagnation point flow, and the detailed investigation of the Navier's stokes equations extracted analytically. The main methodology is given work of PDEs is converted into ODEs using the appropriate similarity transformations. The momentum equations solved analytically to derive the solution domain, the impact of thermal radiation is seen in energy equation, four different scenarios are used to solve the energy equation. Aim of the present work is to study the theoretical analysis and it can be discussed for dual nature behavior by providing different physical parameters, these parameters control the domain, momentum and heat transpiration. In the heat transfer analysis solutions are derived in terms of incomplete gamma function and confluent hypergeometric form. The current work is examined using graphene nanoparticles, and the value of Pr is fixed at 6.2. The present problem is the benchmark solution for the results and it is significance in industrial and technological applications in fluid-based systems involving shrinkable/stretchable materials. At the end we get Velocity decreases with increases of  $V_C$  for upper branch of solution in the case shrinking sheet.

#### 1. Introduction

Numerous researchers are interested in the problem of momentum and heat transfer due to its numerous industrial applications, including polymer extrusion, paper manufacturing, metal cooling, glass blowing, etc., [1]. Sakiadis [2,3] looks at stretching sheet issues initially. Crane [4] extended this issue with a 2-D flow resulting from a stretched sheet that was moving in its own plane at a variable speed. Numerous studies on the issues of stretching sheets have been conducted in part as a result of these works. In the presence of a magnetic field and radiation, Aly [5] studied the 2-D incompressible steady flow with metallic and nonmetallic nanoparticles. Mahabaleshwar et al. [6] explained the theoretical investigation for unsteady flow due to impulsive stretching sheet problem. In the presence of a stretching sheet, Andersson et al. [7,8] investigated the magneto hydrodynamic flow of a power law and viscoelastic fluid. Mahabaleshwar et al. [9-12] examine the MHD effect for different types of fluid flow by using variety of boundary conditions with various physical parameters.

These experiments are restricted to the stretching sheet problems

with different boundary conditions, further the investigations carried out with nanofluids. Most of all agree that nanofluid term is first introduced by Choi [13]. Nanofluids are the mixture of base fluids with nanoparticles. Nanoparticles are added to base fluids to obtain nanofluids. By using these nanofluids many investigations are carried out, Mahabaleshwar et al. [14] studied the nanofluid flow in the presence of magneto hydrodynamics with suction. In order to explain the thermal conductivity and viscosity of nanofluids, Sharifpur et al. [15,16] and Benos et al. [17] developed an asymptotic solution for nanofluid in a porous media that contained three different types of nanofluids: Cu, Al<sub>2</sub>O<sub>3</sub>, and TiO<sub>2</sub>. See some other examples of nanofluids in [40–41]. One of the most beneficial nanomaterials is graphene, which combines two of the best qualities of materials: strength and thinness. For further information, check Reference [18]. Different physical properties and applications of graphene are clearly detailed in the references [19–20]. It is a better thermal and electrical conductor and optically transparent material when compared to other materials The exact solutions of graphene water nanofluid flow across a stretching/shrinking sheet in the presence of suction/injection heat source/sink in the presence of dual nature were also examined by Aly [21]. Additionally, take a look at Singh et al [22].

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Nomenclature		β	Solution domain ( – )				
		ν	Kinematic viscosity $(m^2 s^{-1})$				
b	Constants ( – )	μ	Dynamic viscosity $(kgm^{-1}s^{-1})$				
B(x,t)	Magnetic field strength (Tesla)	ĸ	Thermal conductivity $(W/mK)$				
$C_P$	Specific heat at constant pressure $(Jkg^{-1}K^{-1})$	ξ	A variable ( – )				
G	Graphene ( – )	$\sigma$	Electrical conductivity $(Sm^{-1})$				
$k^*$	Mean absorption coefficient $(-)$	$\sigma^{*}$	$\sigma^*$ Stefan Boltzmann constant ( $Wm^{-2}K^{-4}$ )				
Μ	Kummer's function $(-)$	D	Density $(kgm^{-3})$				
Р	pressure $(Nm^{-2})$	r					
$q_r$	Radiative heat flux $(-)$	Subscript	ipts				
$q_w$	Local heat flux $(Wm^{-2})$	w	Condition at wall $(-)$				
R	Radiation parameter $(-)$	$\infty$	Condition at free stream $(-)$				
$V_C$	Mass transpiration $(-)$	η	Differentiation with respect to $\eta$ ( $-$ )				
Т	Temperature (K)	Abbrevia	hbreviations				
(u, v)	Components of velocities $(ms^{-1})$	MHD Magneto hydrodynamics ( - )					
$(\boldsymbol{x}, \boldsymbol{y})$	Coordinates ( <i>m</i> )	PST	Prescribed surface temperature $(-)$				
$V_w$	Mass transfer velocity $(ms^{-1})$	PHF	Prescribed heat flux ( – )				
Greek symbols							
$\alpha$ Wall moving parameter (-)							



Fig. 1. Schematic diagram of fluid flow.

Based on the aforementioned research, the current work provides an explanation for the unsteady stagnation point flow caused by MHD sheet stretching and contracting along with thermal radiation and mass transpiration. Graphene nanoparticles are used to analyse the present analysis. The main methodology used in the current analysis is the energy equations are also solved under four different cases and represented in terms of incomplete gamma function as well as Kummer's function to provide the solution domain for the resultant ODEs. Analysing the results of the present can be done by employing different regulating parameters. The flow's dual nature can also be verified. It is possible to draw conclusions from the results using graphical representations. Fang et al. are effectively argued in the current study [23]. The scientific contribution of the present work is used in the field of crystal growing, continuous cooling, glass fibre production and entropy generation Also, the significance of nanoparticles with the fluid flow enhanced the convective heat transfer and lowered the friction characteristics, also higher flow rates the heat transfer characteristics and friction decreases.

## 2. Physical model and solution

In order to achieve the current analysis, we are considering the following assumptions it helps to understand the effect on fluid flow.

#### Table 1

Base fluid and nanoparticle thermophysical characteristics (See [30-31]).

	$C_P(J/kgK)$	$ ho \left( kg/m^{3}  ight)$	k(W/mK)	$\sigma(\Omega/m)^{-1}$	Pr
Pure water $(H_2O)$ Graphene(G)	4179 2100	997.1 2250	0.613 2500	$\begin{array}{c} 0.05\\ 1\times 10^7 \end{array}$	6.2

- A laminar MHD two-dimensional unsteady stagnation point flow with a free stream velocity  $U_{\infty} = bxt^{-1}$  is considered in the present analysis, here *b* is constant.
- B(x,t) denotes the strength of magnetic field applied perpendicular to the surface and it is defined by  $B(x,t) = B_0/t$ .
- The physical scenario is schematically represented at Fig. 1. The xaxis moves away towards the free stream direction, and the y-axis runs perpendicular to it.
- Physical quantities of these nanofluids are represented at Table 1.
- $U_w = \frac{abx}{t}$  is x-direction velocity. The temperature at the wall is kept constant at  $T_w$  or with heat flux  $\frac{q_w}{\sqrt{t}}$ .  $T_\infty$  is the constant temperature of the free stream fluid.
- The governing 2-D Navier's stokes equation is given by (See Mahabaleshwar et al. [23], Anusha et.al.[24], Bhatti et al. [32], Hassan et al. [33]).

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \tag{1}$$

$$\rho_{nf}\left(\frac{\partial u}{\partial t} + u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y}\right) = -\frac{\partial P}{\partial x} + \mu_{nf}\left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2}\right) + \sigma_{nf}B^2(x,t)(U_{\infty} - u)$$
(2)

$$\rho_{nf}\left(\frac{\partial v}{\partial t} + u\frac{\partial v}{\partial x} + v\frac{\partial v}{\partial y}\right) = -\frac{\partial P}{\partial y} + \mu_{nf}\left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2}\right)$$
(3)

$$(\rho C_P)_{nf} \left( \frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \right) = \kappa_{nf} \left( \frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right) - \frac{\partial q_r}{\partial y}$$
(4)

the suitable boundary conditions as

$$\begin{array}{c} u(x,0,t) = \frac{\alpha b x}{t}, \\ v(x,0,t) = V_w(x,t), \\ u(x,\infty,t) = \frac{b x}{t} \end{array} \right\}$$

$$(5)$$

$$T = T_w, \quad T \to T_\infty \quad \text{for PST case} \\ -\kappa \frac{\partial T}{\partial y} = \frac{q_w}{\sqrt{t}}, \quad T \to T_\infty \quad \text{for PHF case} \end{cases}$$
(6)

The Nomenclature contains definitions of the terms used in Eqs. (1) to (6).

Similarity variables can be defined as

$$\psi(x, y, t) = bf(\eta)x\sqrt{\frac{\nu}{t}}\eta = \frac{y}{\sqrt{\nu t}}, \theta(\eta) = \frac{T - T_{\infty}}{T_w - T_{\infty}}$$
(7)

These are the components of velocity that can be defined using the stream function:

$$u = \frac{bx}{t} f_{\eta}(\eta), \quad v = -b\sqrt{\frac{\nu}{t}} f(\eta)$$
(8)

The velocity of wall transpiration is also provided by

$$V_{w}(x,t) = V_{w}(t) = -b\sqrt{\frac{\nu}{t}}f(0)$$
(9)

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## 3. Solution of pressure term

The term  $\frac{\partial P}{\partial y}$  is the function of t and y it can be calculated by Eq.(3), it means  $\frac{\partial P}{\partial y} = \Phi(t, y)$ , the integration of this derivative yields to get the following result

$$\mathbf{P} = \int \phi(t, y) + \psi(t, x) \tag{10}$$

here,  $\psi(t, x)$  is constant of integration.

Again differentiate Eq. (10) to get the equation as  $\frac{\partial P}{\partial x} = \frac{\partial \psi(t,x)}{\partial x}$ , this is free from *y*. then applying *x*-momentum with  $u = U_{\infty}, \frac{\partial P}{\partial x}$  can be derived as

$$-\frac{1}{\rho_{nf}}\frac{\partial P}{\partial x} = \frac{\partial U_{\infty}}{\partial t} + U_{\infty}\frac{\partial U_{\infty}}{\partial x} = -\frac{bx}{t^2} + \frac{b^2x}{t^2}$$
(11)

The pressure gradient in the y-direction is similarly provided by

$$-\frac{1}{\rho_{nf}}\frac{\partial P}{\partial y} = \frac{\partial v}{\partial t} + v\frac{\partial v}{\partial y} - \nu_{nf}\frac{\partial^2 v}{\partial y^2}$$
(12)

The pressure can be derived from integrating Eq. (11) and (12), then the equation becomes

$$\frac{1}{\rho_{nf}}(P_0 - P) = -\frac{bx^2}{2t^2} + \frac{b^2x^2}{2t^2} + \frac{b\nu}{2t}f(\eta)\eta + \frac{b^2\nu_f}{2t}f_\eta(\eta) + \frac{b\nu_{nf}}{t}f_\eta(\eta)$$
(13)

where,  $P_0$  is constant obtained from the integration.

## 4. Exact solution for velocity

The following can be obtained by applying the similarity variables defined at Eqs. (7) and (8) in Eq. ODE

$$\frac{\varepsilon_1}{\varepsilon_2}f_{\eta\eta\eta} + \left(bf + \frac{\eta}{2}\right)f_{\eta\eta} + (1 - bf_\eta)f_\eta + (b - 1) + \frac{\varepsilon_3}{\varepsilon_2}bQ(1 - f_\eta) = 0$$
(14a)

The boundary condition associated with this equation also reduced as

$$f_{\eta}(0) = \alpha, \ f(0) = V_C, \ f_{\eta}(\infty) = 1$$
 (14b)

Here,  $\alpha = \frac{U_w}{U_\infty}$  is the wall stretching parameter,  $Q = \frac{\sigma_f B_0^2}{\rho_f bt}$  is the Chandrasekhar's number,  $V_C = -\frac{V_w(x,t)}{b\sqrt{\nu/t}}$  represents mass transpiration, and the values of *b* determine mass transpiration.

We now explore a unique case considering b = -1/2, in Eq.(14a), then we yield

$$\frac{\varepsilon_1}{\varepsilon_2} f_{\eta\eta\eta} + \left(-\frac{1}{2}f + \frac{\eta}{2}\right) f_{\eta\eta} + \left(1 + \frac{1}{2}f_\eta\right) f_\eta + \left(-\frac{1}{2} - 1\right) + \frac{\varepsilon_3}{\varepsilon_2} \left(-\frac{1}{2}\right) Q(1 - f_\eta)$$

$$= 0$$
(15)

Defining a new transformation  $F(\eta) = f(\eta) - \eta$ , substituting this transformation in Eq. (15), then it becomes

$$\varepsilon_1 F_{\eta\eta\eta} - \frac{\varepsilon_2}{2} F F_{\eta\eta} + 2\varepsilon_2 F_{\eta} + \frac{\varepsilon_2}{2} F_{\eta}^2 - \frac{\varepsilon_3}{2} Q F_{\eta} = 0$$
(16)

Eq. (14) of the corresponding boundary conditions also reduces to

$$F(0) = V_C, \quad F_\eta(0) = \alpha - 1, \quad F_\eta(\infty) = 0$$
 (17)

Assume Eq. (16) has a solution that takes the form

$$F(\eta) = c + dExp(-\beta\eta)$$
(18)

By using Boundary conditions defined at Eq. (17) the following results can be found

$$d = \frac{1-\alpha}{\beta}, \quad c = V_C + \frac{1-\alpha}{\beta} \tag{19}$$



(b)

a

**Fig. 2.**  $\beta$  verses  $\alpha$  for different  $V_C$  values.





(b)

**Fig. 3.**  $f_{\eta}(\eta)$  verses  $\eta$  for various  $V_C$  values at different  $\alpha$ .



**Fig. 4.**  $f_{\eta}(\eta)$  verses  $\eta$  for different choices of  $V_C$ .



Fig. 5. Streamline patterns at different time for lower branch of solution.









Fig. 6. streamline patterns at different time for upper branch of solution.

Also we got

$$2\varepsilon_1\beta^2 + \varepsilon_2 V_C\beta + (\varepsilon_2(\alpha+3) - 2\varepsilon_3 Q) = 0$$
<sup>(20)</sup>

The answer to this quadratic equation is as follows.

$$\beta = \frac{-\varepsilon_2 V_C + \sqrt{(\varepsilon_2 V_C)^2 - 8\varepsilon_1(\varepsilon_2(\alpha + 3) - 2\varepsilon_2)}}{4\varepsilon_1}$$
(21)

here,  $\beta$  must be positive value for physically feasible solution. Based on Eq. (20) the real roots can be yield only when the  $V_C$  and  $\alpha$  must satisfy  $(\varepsilon_2 V_C)^2 - 8\varepsilon_1(\varepsilon_2(\alpha + 3) - 2\varepsilon_2) \ge 0$ . It is observed that there are two solutions for Eq.(20) for certain values of  $V_C$  and  $\alpha$ . The general solution for Eq.(15) is given for upper solution branch

$$f(\eta) = \eta + V_C + \frac{4\varepsilon_1(1-\alpha)}{-\varepsilon_2 V_C + \sqrt{\sqrt{(\varepsilon_2 V_C)^2 - 8\varepsilon_1(\varepsilon_2(\alpha+3) - 2\varepsilon_2)}}} \times \left( Exp\left( -\frac{-\varepsilon_2 V_C + \sqrt{\sqrt{(\varepsilon_2 V_C)^2 - 8\varepsilon_1(\varepsilon_2(\alpha+3) - 2\varepsilon_2)}}}{4\varepsilon_1} \eta \right) - 1 \right)$$

$$(22)$$

And for the lower solution branch is given by

$$f(\eta) = \eta + V_C + \frac{4\varepsilon_1(1-\alpha)}{-\varepsilon_2 V_C - \sqrt{\sqrt{(\varepsilon_2 V_C)^2 - 8\varepsilon_1(\varepsilon_2(\alpha+3) - 2\varepsilon_2)}}} \times \left( Exp\left( -\frac{-\varepsilon_2 V_C - \sqrt{\sqrt{(\varepsilon_2 V_C)^2 - 8\varepsilon_1(\varepsilon_2(\alpha+3) - 2\varepsilon_2)}}}{4\varepsilon_1} \eta \right) - 1 \right)$$

$$(23)$$

And the velocity for upper and lower branch solution is given by

$$f(\eta) = 1 + (\alpha - 1) Exp\left( -\frac{-\varepsilon_2 V_C + \sqrt{\sqrt{(\varepsilon_2 V_C)^2 - 8\varepsilon_1(\varepsilon_2(\alpha + 3) - 2\varepsilon_2)}}}{4\varepsilon_1}\eta \right)$$
(24)

$$f(\eta) = 1 + (\alpha - 1)Exp\left(-\frac{-\varepsilon_2 V_C + \sqrt{\sqrt{(\varepsilon_2 V_C)^2 - 8\varepsilon_1(\varepsilon_2(\alpha + 3) - 2\varepsilon_2)}}}{4\varepsilon_1}\eta\right)$$
(25)

# 5. Analytical solution of energy equation

Applying the similarity variables to Eq. (4), we obtain the following ODE  $\$ 

$$(\varepsilon_5 + R)\theta_{\eta\eta} + Pr\varepsilon_4 \left(\frac{\eta}{2} + bf\right)\theta_{\eta} = 0$$
(26)

For the PST and PHF cases, the boundary conditions associated with this energy equation are reduced to the following form.

$$\begin{array}{l} \theta(0) = 1, \ \theta(\infty) \rightarrow 0 \quad \text{for PST case} \\ h_{\eta}(0) = -1, \ h(\infty) \rightarrow 0 \quad \text{for PHF case} \end{array} \right\}$$

$$(27a,b)$$

here, 
$$Pr = \frac{(\mu C_P)_f}{\kappa_f}$$
 is Prandtl number,  $R = \frac{16\sigma^2 T_{\infty}^2}{3K_f k^2}$  is the radiation

parameter, it is computed with the use of Rosseland's approximation, using this estimation  $q_r$  is modelled as  $q_r = -\frac{4\sigma^2}{3k^2} \frac{\partial T^4}{\partial y}$ , then it is possible to expand the word  $T^4$  using Taylor's series while disregarding higher order terms to obtain  $T^4 = -3T_{\infty}^3 + 4T_{\infty}^3 T$ . on substituting these terms into Eq. (4) to get  $\frac{\partial q_r}{\partial y} = -\frac{16\sigma^2 T_{\infty}^3}{3k^2} \frac{\partial^2 T}{\partial y^2}$ , by using this the thermal radiation *R* can be calculated (See Mahabaleshwar et al. [25–27,34–36]). Also nanofluid quantities  $\varepsilon_1$  to  $\varepsilon_5$  used in Eq.(14) and (26) is given by (See [28–29,37–39])

$$\epsilon_1 = \frac{\mu_{nf}}{\mu_f} = \frac{1}{(1-\phi)^{2.5}}$$
(28a)

$$e_2 = \frac{\rho_{nf}}{\rho_f} = 1 - \phi + \phi \frac{\rho_s}{\rho_f}$$
(28b)

$$\sigma_{3} = \frac{\sigma_{nf}}{\sigma_{f}} = 1 + \frac{3\left(\frac{\sigma_{s}}{\sigma_{f}} - 1\right)\phi}{\left(\frac{\sigma_{s}}{\sigma_{f}} + 2\right) - \left(\frac{\sigma_{s}}{\sigma_{f}} - 1\right)\phi}$$
(28c)

$$\varepsilon_4 = \frac{(\rho C_p)_{nf}}{(\rho C_p)_f} = 1 - \phi + \phi \frac{(\rho C_p)_s}{(\rho C_p)_f}$$
(28d)

$$\varepsilon_{5} = \frac{\kappa_{nf}}{\kappa_{f}} = \frac{\kappa_{s} + 2\kappa_{f} + 2\phi(\kappa_{s} - \kappa_{f})}{\kappa_{s} + 2\kappa_{f} - \phi(\kappa_{s} - \kappa_{f})}.$$
(28e)

Then by using Eq.(20) the term  $V_c$  can be obtained as

$$V_C = \frac{-2\varepsilon_1}{\varepsilon_2}\beta - \frac{(\varepsilon_2(\alpha+3) - 2\varepsilon_3Q)}{\beta\varepsilon_2}$$
(29)

## 5.1. Constant wall temperature case (PST case)

By using Eq. (29) the energy equation can be altered as

$$(\varepsilon_5 + R)\theta_{\eta\eta} - \frac{1}{2}Pr\varepsilon_4 \left( V_C - \frac{(1-\alpha)}{\beta} + \frac{(1-\alpha)}{\beta} Exp(-\beta\eta) \right) \theta_{\eta} = 0$$
(30)

Introducing a new variable  $\xi$  as

$$\xi = (1 - \alpha) \frac{Pr}{2\beta^2} Exp(-\beta\eta)$$
(31)

using new transformation  $\xi$  and  $V_C$  in Eq.(30) to yield the following resulting equation

$$\xi(\varepsilon_5+R)\frac{\partial^2\theta}{\partial\xi^2} + \left((\varepsilon_5+R) - \varepsilon_4 Pr\left(\frac{\varepsilon_1}{\varepsilon_2} + \frac{2\varepsilon_2 - \varepsilon_3 Q}{\beta^2}\right) + \varepsilon_4 \xi\right)\frac{\partial\theta}{\partial\xi} = 0 \quad (32)$$

Boundary conditions associated with PST case is also reduces to

$$\theta\left(\frac{Pr(1-\alpha)}{2\beta^2}\right) = 1, \ \theta(0) = 0 \tag{33}$$

Then the general solution of Eq. (32) gives as

$$\theta(\xi) = C_1 + C_2 \frac{\frac{Pr}{(\varepsilon_5 + R)} \left(\frac{\varepsilon_1}{\varepsilon_2} + \frac{2\varepsilon_2 - \varepsilon_3 Q}{\beta^2}\right)}{\varepsilon_4^{\frac{Pr}{(\varepsilon_5 + R)} \left(\frac{\varepsilon_1}{\varepsilon_2} + \frac{2\varepsilon_2 - \varepsilon_3 Q}{\beta^2}\right)}}$$
$$\Gamma\left(\frac{Pr}{(\varepsilon_5 + R)} \left(\frac{\varepsilon_1}{\varepsilon_2} + \frac{2\varepsilon_2 - \varepsilon_3 Q}{\beta^2}\right), 0\right) - \Gamma\left(\frac{Pr}{(\varepsilon_5 + R)} \left(\frac{\varepsilon_1}{\varepsilon_2} + \frac{2\varepsilon_2 - \varepsilon_3 Q}{\beta^2}\right), \varepsilon_4 \xi\right)$$
(34)

By using the boundary condition defined at Eq.(27a) in Eq. (34) to yield the following result

$$\theta(\eta) = \frac{\Gamma\left[\frac{Pr}{(\epsilon_{5}+R)}\left(\frac{\epsilon_{1}}{\epsilon_{2}} + \frac{2\epsilon_{2}-\epsilon_{3}Q}{\beta^{2}}\right), 0\right] - \Gamma\left[\frac{Pr}{(\epsilon_{5}+R)}\left(\frac{\epsilon_{1}}{\epsilon_{2}} + \frac{2\epsilon_{2}-\epsilon_{3}Q}{\beta^{2}}\right), \epsilon_{4}\frac{(1-\alpha)Pr}{2\beta^{2}}Exp(-\beta\eta)\right]}{\Gamma\left[\frac{Pr}{(\epsilon_{5}+R)}\left(\frac{\epsilon_{1}}{\epsilon_{2}} + \frac{2\epsilon_{2}-\epsilon_{3}Q}{\beta^{2}}\right), 0\right] - \Gamma\left[\frac{Pr}{(\epsilon_{5}+R)}\left(\frac{\epsilon_{1}}{\epsilon_{2}} + \frac{2\epsilon_{2}-\epsilon_{3}Q}{\beta^{2}}\right), \epsilon_{4}\frac{(1-\alpha)Pr}{2\beta^{2}}\right]}$$
(35)

then the wall's heat flux is determined by

$$\theta_{\eta}(0) = \frac{-\beta \left(\frac{(1-a)Pr}{2\beta^2}\right)^{\frac{Pr}{(\epsilon_{5}+R)}\left(\frac{\epsilon_{1}}{2\gamma}+\frac{2\epsilon_{2}-\epsilon_{3}Q}{\beta^2}\right)}}{\Gamma\left[\frac{Pr}{(\epsilon_{5}+R)}\left(\frac{\epsilon_{1}}{\epsilon_{2}}+\frac{2\epsilon_{2}-\epsilon_{3}Q}{\beta^2}\right), \ 0\right] - \Gamma\left[\frac{Pr}{(\epsilon_{5}+R)}\left(\frac{\epsilon_{1}}{\epsilon_{2}}+\frac{2\epsilon_{2}-\epsilon_{3}Q}{\beta^2}\right), \ \epsilon_{4}\frac{(1-a)Pr}{2\beta^{2}}\right]}$$
(36)

#### 5.2. Uniform heat flux case

Defining  $h(\eta) = \frac{T-T_{\infty}}{\frac{dw}{dw} \sqrt{\nu}}$ , adding this to the energy equation will provide the following equation:

$$(\varepsilon_5 + R)h_{\eta\eta} + \frac{1}{2}\varepsilon_4 Pr(\eta - f)h_\eta = 0$$
(37)

using solution of momentum in Eq. (37) to yield

$$(\varepsilon_5 + R)h_{\eta\eta} - \frac{1}{2}Pr\varepsilon_4 \left(V_C - \frac{(1-\alpha)}{\beta} + \frac{(1-\alpha)}{\beta}Exp(-\beta\eta)\right)h_{\eta} = 0$$
(38)

Since Eq. (38) and Eq. (30) are comparable, and Eq. (34) and Eq. (30) have the same solution, the general answer to Eq. (38) is obtained as

$$h(\xi) = C_1 + C_2 \frac{\frac{Pr}{(\varepsilon_5 + R)} \left(\frac{\varepsilon_1}{\varepsilon_2} + \frac{2\varepsilon_2 - \varepsilon_3 Q}{\beta^2}\right)}{\varepsilon_4^{\frac{Pr}{(\varepsilon_5 + R)} \left(\frac{\varepsilon_1}{\varepsilon_2} + \frac{2\varepsilon_2 - \varepsilon_3 Q}{\beta^2}\right)}}$$
$$\Gamma\left(\frac{Pr}{(\varepsilon_5 + R)} \left(\frac{\varepsilon_1}{\varepsilon_2} + \frac{2\varepsilon_2 - \varepsilon_3 Q}{\beta^2}\right), 0\right) - \Gamma\left(\frac{Pr}{(\varepsilon_5 + R)} \left(\frac{\varepsilon_1}{\varepsilon_2} + \frac{2\varepsilon_2 - \varepsilon_3 Q}{\beta^2}\right), \varepsilon_4 \xi\right)$$
(39)

By incorporating the boundary conditions from Eq. (27b) into Eq. (39), the following equation is produced.

$$h(\eta) = \frac{\Gamma\left[\frac{Pr}{(\epsilon_{5}+R)}\left(\frac{\epsilon_{1}}{\epsilon_{2}} + \frac{2\epsilon_{2}-\epsilon_{3}Q}{\beta^{2}}\right), 0\right] - \Gamma\left[\frac{Pr}{(\epsilon_{5}+R)}\left(\frac{\epsilon_{1}}{\epsilon_{2}} + \frac{2\epsilon_{2}-\epsilon_{3}Q}{\beta^{2}}\right), \epsilon_{4}\frac{(1-a)Pr}{2\beta^{2}}Exp(-\beta\eta)}{\beta\left(\frac{(1-a)Pr}{2\beta^{2}}\right)^{\frac{Pr}{(\epsilon_{5}+R)}\left(\frac{\epsilon_{1}}{\epsilon_{2}} + \frac{2\epsilon_{2}-\epsilon_{3}Q}{\beta^{2}}\right)}Exp\left(-\frac{(1-a)Pr}{2\beta^{2}}\right)}$$

$$(40)$$

Given as follows is the dimensionless wall heat flux:

$$h(0) = \frac{\Gamma\left[\frac{P_r}{(\epsilon_5+R)}\left(\frac{\epsilon_1}{\epsilon_2} + \frac{2\epsilon_2 - \epsilon_3 Q}{\beta^2}\right), \ 0\right] - \Gamma\left[\frac{P_r}{(\epsilon_5+R)}\left(\frac{\epsilon_1}{\epsilon_2} + \frac{2\epsilon_2 - \epsilon_3 Q}{\beta^2}\right), \ \varepsilon_4 \frac{(1-\alpha)P_r}{2\beta^2}\right]}{\beta\left(\frac{(1-\alpha)P_r}{2\beta^2}\right)^{\frac{P_r}{(\epsilon_5+R)}\left(\frac{\epsilon_1}{\epsilon_2} + \frac{2\epsilon_2 - \epsilon_3 Q}{\beta^2}\right)} Exp\left(-\frac{(1-\alpha)P_r}{2\beta^2}\right)}$$
(41)

On the analysis of this result, it is observed that  $h(0) = -\frac{1}{\theta_{\eta}(0)}$ .

#### 5.3. Power law wall temperature for general case

The conditions used in the above literature is very rare to investigate the temperature at wall. But in this section we discussed the general situation by taking power law depended on both time and distance and it is given by

$$T = T_{\infty} + (T_w - T_{\infty})x^n t^m \theta(\eta)$$
(42)

The boundary conditions associated with Eq. (43) as

$$\theta(0) = 1, \ \theta(\infty) = 0 \tag{44}$$

Put b = -1/2 in Eq.(43), then Eq.(43) becomes

$$(\varepsilon_5 + R)\theta_{\eta\eta} + \varepsilon_4 \frac{Pr}{2}(\eta - f)\theta_\eta + \varepsilon_4 \frac{Pr}{2}(\eta f_\eta - 2m)\theta = 0$$
(45)

using  $\xi = \frac{(\alpha-1)}{2Pr\beta^2} Exp(-\beta\eta)$  in Eq.(45) to yield as

$$\xi(\varepsilon_5 + R)\frac{\partial^2\theta}{\partial\xi^2} + \left((\varepsilon_5 + R) - A - \xi\right)\frac{\partial\theta}{\partial\xi} + \left(\frac{B}{\xi} + n\right)\theta = 0$$
(46)

here,  $A = Pr\epsilon_4 \left(1 + \frac{2\epsilon_2 - \epsilon_3 M}{\beta^2}\right), \quad B = \frac{1}{\beta^2} Pr\epsilon_4 \left(\frac{n}{2} - m\right).$ Boundary conditions defined in Eq. (44) reduces as

$$\theta\left(\frac{Pr(\alpha-1)}{2\beta^2}\right) = 1, \ \theta(0) = 0 \tag{47}$$

Now we define

$$\theta(\xi) = \xi^{\delta} \psi(\xi) \tag{48}$$

On applying Eq. (48) in Eq. (46), then it transformed as

$$\xi(\varepsilon_5+R)\frac{\partial^2\psi}{\partial\xi^2} + (\gamma-\xi)\frac{\partial\psi}{\partial\xi} + \left\{\frac{1}{\xi}\left(\delta^2(\varepsilon_5+R) - A\delta + B\right) - \delta + n\right\}\psi(\xi) = 0$$
(49)

here,  $\delta = \frac{A \pm \sqrt{A^2 - 4B(\varepsilon_5 + R)}}{2(\varepsilon_5 + R)}$ , which requires  $A^2 - 4B(\varepsilon_5 + R) \ge 0$ , and  $\frac{Pr\epsilon_4}{2}(\beta^2 \varepsilon_1 + 2\varepsilon_2 - \varepsilon_3 Q)^2 \ge 2n - 4m$ , with  $\omega = \delta - n$ .

Therefore, Eq. (49) becomes

$$\xi(\varepsilon_5 + R)\frac{\partial^2 \psi}{\partial \xi^2} + (\gamma - \xi)\frac{\partial \psi}{\partial \xi} - \omega \psi(\xi) = 0$$
(50)

Given that Eq. (50) is a basic confluent hypergeometric differential equation, the following is its solution:

$$\psi(\xi) = C_1 M\left(\omega, \gamma, \frac{\xi}{(\varepsilon_5 + R)}\right)$$
(51)

By using the boundary condition  $\theta(0) = 1$  the constant  $C_1$  can be determined

$$C_1 = \frac{\left((\alpha - 1)\frac{Pr}{2\beta^2}\right)^{-\delta}}{M\left(\omega, \gamma, \frac{(\alpha - 1)Pr}{2(\varepsilon_5 + R)\beta^2}\right)}$$
(52)

then using  $\psi(\xi)$  in Eq.(48) to yield the result as

$$\theta(\eta) = \frac{Exp(-\beta\delta\eta)M\left(\delta - n, \gamma, \frac{(\alpha-1)Pr}{2(\epsilon_5 + R)\beta^2}Exp(-\beta\eta)\right)}{M\left(\delta - n, \gamma, \frac{(\alpha-1)Pr}{2(\epsilon_5 + R)\beta^2}\right)}$$
(53)

The wall heat flux is then presented as

$$-\theta_{\eta}(0) = \delta\beta + \frac{(\alpha - 1)(\delta - n)Pr}{\beta(\varepsilon_{5} + R)(2(\varepsilon_{5} + R) - A + 2\delta(\varepsilon_{5} + R))} \frac{M\left(\delta - n + 1, \gamma + 1, \frac{(\alpha - 1)Pr}{2(\varepsilon_{5} + R)\beta^{2}}\right)}{M\left(\delta - n, \gamma, \frac{(\alpha - 1)Pr}{2(\varepsilon_{5} + R)\beta^{2}}\right)}$$
(54)

The following ODE, which has no relation to Eq. (4), is obtained by substituting this new definition into Eq. (26)

$$(\varepsilon_5 + R)\theta_{\eta\eta} + \varepsilon_4 Pr\left(bf + \frac{1}{2}\eta\right)\theta_\eta - \varepsilon_4 Pr(bnf_\eta + m)\theta = 0$$
(43)

#### 5.4. Power law heat flux for general case

Let us assume that power law heat flux at wall heat flux depended on both time and distance as



**Fig. 7.** Impact of  $\theta(\eta)$  on  $\eta$  for various  $\alpha$  values at (a) injection ( $V_C < 0$ )(b) no permeability ( $V_C = 0$ ) and (c) suction ( $V_C > 0$ ).

$$-\kappa \frac{\partial T}{\partial y} = q_w x^n t^{m-\frac{1}{2}}$$
(55)

therefore, dimensionless temperature is given by

$$T = T_{\infty} + \frac{q_w}{\kappa} \sqrt{\nu} x^n t^m h(\eta)$$
(56)

when this is substituted into Equation (4), the resulting equation is

$$(\varepsilon_5 + R)h_{\eta\eta} + \varepsilon_4 Pr\left(bf + \frac{1}{2}\eta\right)h_\eta - \varepsilon_4 Pr(bnf_\eta + m)h = 0$$
(57)

consider b = -1/2 in Eq.(57) then it is changed as



**Fig. 8.** Impact of  $\theta(\eta)$  on  $\eta$  for various  $V_C$  values at (a)  $\alpha = -4$ (b)  $\alpha = -6$ (c)  $\alpha = -10$  and (d)  $\alpha = -12$ .

$$(\varepsilon_{5}+R)h_{\eta\eta}+\varepsilon_{4}\frac{Pr}{2}(\eta-f)h_{\eta}+\varepsilon_{4}\frac{Pr}{2}(\eta f_{\eta}-2m)h=0$$
(58)

The associated boundary conditions of Eq. (58) reduced to

$$h_{\eta}(0) = -1, \ h(\infty) \rightarrow 0 \tag{59}$$

Since Eq. (58) is similar to Eq. (45) in this case and the answer up to Eq. (51) is identical to Eq. (45), the solution to Eq. (58) is given by

$$\psi(\xi) = C_1 M\left(\omega, \gamma, \frac{\xi}{(\varepsilon_5 + R)}\right)$$
(60)

The boundary conditions stated in Eq. (59) allow the determination of  ${\cal C}_1$ 



**Fig. 9.** Impact of  $-\theta_{\eta}(0)$  on *R*, as a function of (a)  $V_C(b)$  *Pr*.

$$C_{1} = \frac{\left(\frac{(\alpha-1)Pr}{2\beta^{2}}\right)^{-1}}{\left\{\delta\beta M\left(\omega, \gamma, \frac{(\alpha-1)Pr}{2(\epsilon_{S}+R)\beta^{2}}\right) + \frac{\omega Pr(\alpha-1)}{2\beta\gamma}M\left(\omega+1, \gamma+1, \frac{(\alpha-1)Pr}{2(\epsilon_{S}+R)\beta^{2}}\right)\right\}}$$
(61)

Using  $C_1$  in Eq. (60) to get

$$h(\eta) = \frac{Exp(-\beta\delta\eta)M\left(\omega, \gamma, \frac{(\alpha-1)Pr}{2(\varepsilon_{5}+R)\beta^{2}}Exp(-\beta\eta)\right)}{\left\{\delta\beta M\left(\omega, \gamma, \frac{(\alpha-1)Pr}{2(\varepsilon_{5}+R)\beta^{2}}\right) + \frac{\omega Pr(\alpha-1)}{2\rho_{T}}M\left(\omega+1, \gamma+1, \frac{(\alpha-1)Pr}{2(\varepsilon_{5}+R)\beta^{2}}\right)\right\}}$$

$$h(0) = \frac{M\left(\omega, \gamma, \frac{(\alpha-1)Pr}{2(\varepsilon_{5}+R)\beta^{2}}\right)}{\left\{\delta\beta M\left(\omega, \gamma, \frac{(\alpha-1)Pr}{2(\varepsilon_{5}+R)\beta^{2}}\right) + \frac{\omega Pr(\alpha-1)}{2\rho_{T}}M\left(\omega+1, \gamma+1, \frac{(\alpha-1)Pr}{2(\varepsilon_{5}+R)\beta^{2}}\right)\right\}}$$

$$(63)$$

## 6. Results and discussion

Results obtained from the 2-D unsteady fluid flow with transpiration and radiation is analysed using different controlling parameters. Velocity equation is solved exactly to yield solution domain, here the dual nature characteristics. This domain helps to solve the heat equation and also put this in terms of incomplete gamma function and also in terms of confluent hypergeometric equation.

#### 6.1. Discussion for flow problem

The plots of  $\beta$  verses  $\alpha$  for different  $V_C$  at Q = 0 and Q = 1 respectively studied at Fig. 2a and b, here domain move towards the positive values of  $\alpha$  if we decreases the values of mass transpiration V<sub>C</sub>. The solution domain is little bit more value for Q = 1, compare to Q = 0. For  $V_C \ge 0$ , there is one solution for  $\alpha = -3$ . The flow problem exist two solution for  $V_C < 0$ . Fig. 3a and b represents the effect of  $f_n(\eta)$  on  $\eta$  for different V<sub>C</sub>, at  $\alpha = -4$ , and  $\alpha = -8$ , respectively. These two plots represent the shrinking sheet case because  $\alpha < 0$  here the velocity decays on raising the  $V_C$  values. Impact of mass transpiration  $V_C$  on velocity is represented at Fig. 4a and b for upper branch of solution(ubs) and lower branch of solution (lbs) respectively, red lines depict ubs and black lines depict *lbs*. Fig. 4a indicates shrinking sheet case because  $\alpha =$ -1, here velocity decays on raising the values of  $V_c$  for upper branch of solution and increases with increases of  $V_C$  for lower branch of solution. Similarly, Fig. 4b depict the stretching sheet case because  $\alpha = 2$ . In this velocity increases with increase of  $V_C$  for upper branch of solution and decreases with increase of  $V_C$  for lower branch of solution. In these figures dotted lines for  $\phi = 0$ , and solid lines for  $\phi = 0.1$ . Fig. 5a to d depict the pattern of stream lines for lower branch of solution at varying time. On the basis of the definitions the formula of stream function is given by

$$\psi(x, y, t) = -\frac{1}{2}f\left(\frac{y}{t}\right)x\sqrt{\frac{1}{t}}$$

Fig. 6a–d depict the pattern of stream lines for upper branch of solution at different time. From these two branches it is cleared that stagnation points of upper and lower solution branch moving away from the wall.

#### 6.2. Discussion for energy equation

Energy equation is discussed under four different cases, these cases are examined analytically, these analytical results are verified with graphical arrangements. Figs. 7–9 graphs are related to constant wall temperature case. Fig. 7a–c depicts the plots of  $\theta(\eta)$  verses  $\eta$  for different  $\alpha$  values respectively at injection ( $V_C < 0$ ), no-permeability ( $V_C = 0$ ) and suction ( $V_C > 0$ ). Here  $\theta(\eta)$  raises for raising the values of  $\alpha$  for all the cases of injection, no-permeability and suction. The boundary value thickness is more wider for large values of  $V_C$ . Effect of  $\theta(\eta)$  on  $\eta$  for various choices of  $V_C$  at different  $\alpha = -4, -6, -10, -12$  respectively indicated at Fig. 8a–d. Here  $\theta(\eta)$  raises for raising the values of  $V_C$ . Fig. 9a–b depicts the effect of  $-\theta_{\eta}(0)$  on R as a function of  $V_C$  and Pr, respectively. In both conditions the value of R more for more values of P



**Fig. 10.**  $h(\eta)$  verses  $\eta$  for various  $\alpha$  values at (a) injection (b) no permeability and (c) suction.

and  $V_C$ , also the value of  $-\theta_{\eta}(0)$  increases with decreases the values of R. Fig. 10a to c are related to the uniform heat flux case, these graphs portrays plots of  $h(\eta)$  on  $\eta$  for various choices of  $\alpha$  at injection ( $V_C < 0$ ), no-permeability ( $V_C = 0$ ) and suction ( $V_C > 0$ ) cases respectively. In all the three cases  $h(\eta)$  increases for increases the values of  $\alpha$ . Fig. 11 exhibit the result of general power-law walls temperature case, it is mathematically represented at Eq. (53). Fig. 11a–c portrays general power-law surface temperature  $\theta(\eta)$  on  $\eta$  for different values of m, at n = -15, -10, -5 respectively. From these figures it is cleared that the values of m decays the temperature profile value, also boundary value thickness is more wider for more values of n.

## 7. Concluding remarks

The current work investigates the two-dimensional unsteady stagnation point flow with G- $H_2O$  nanoparticles. Velocity and heat equations solved exactly, then the heat equation solved under PST and PHF conditions. The energy equations are also solved under four different cases and represented in terms of incomplete gamma function as well as Kummer's function to provide the solution domain for the resultant ODEs. Analysing the results of the present can be done by employing different regulating parameters. The flow's dual nature can also be verified. It is possible to draw conclusions from the results using graphical representations. At the end we get the following results.

- The solution domain of the momentum equation containing two branches of solution namely upper and lower branches.
- Domain value raises for raising the  $V_C$  values. Here domain is little bit more value for Q = 1, compare to Q = 0.
- Velocity decreases with increases of *V*<sub>C</sub> for *ubs* and increases with increases of *V*<sub>C</sub> for lower branch of solution in the case shrinking sheet.
- Velocity decreases with increases of *V<sub>C</sub>* for upper branch of solution and increases with increases of *V<sub>C</sub>* for lower branch of solution in the case of stretching sheet.



**Fig. 11.** Impact of general power-law surface temperature  $\theta(\eta)$  on  $\eta$  for various *m* values at (a) n = -15(b) n = -10 and (c) n = -5.

- $\theta(\eta)$  raises for raising  $\alpha$  and  $V_C$  values for all the cases of injection, nopermeability and suction.
- In the case constant power law wall temperature the value of *R* decays on raising *Pr* and *V*<sub>*C*</sub>, also the value of  $-\theta_{\eta}(0)$  increases with decreases the values of *R*
- $h(\eta)$  raises for raising the values of  $\alpha$  in the case of uniform heat flux case.
- In the case of general power-law walls temperature, values of *m* decreases the temperature profile value.

# CRediT authorship contribution statement

**A.B. Vishalakshi:** Conceptualization, Investigation, Methodology, Writing – review & editing. **U.S. Mahabaleshwar:** Supervision, Conceptualization, Methodology, Formal analysis, Writing – original draft. **L.M. Pérez:** Methodology, Writing – review & editing. **O. Manca:** Supervision, Methodology, Writing – review & editing.

#### **Declaration of Competing Interest**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

## Data availability

Data will be made available on request.

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